

Centre for Research & Technology Hellas Chemical Process & Energy Resources Institute



Techno-economic and Environmental Considerations for Aviation and Marine Fuels Production from Biomass Derived Microbial Oil

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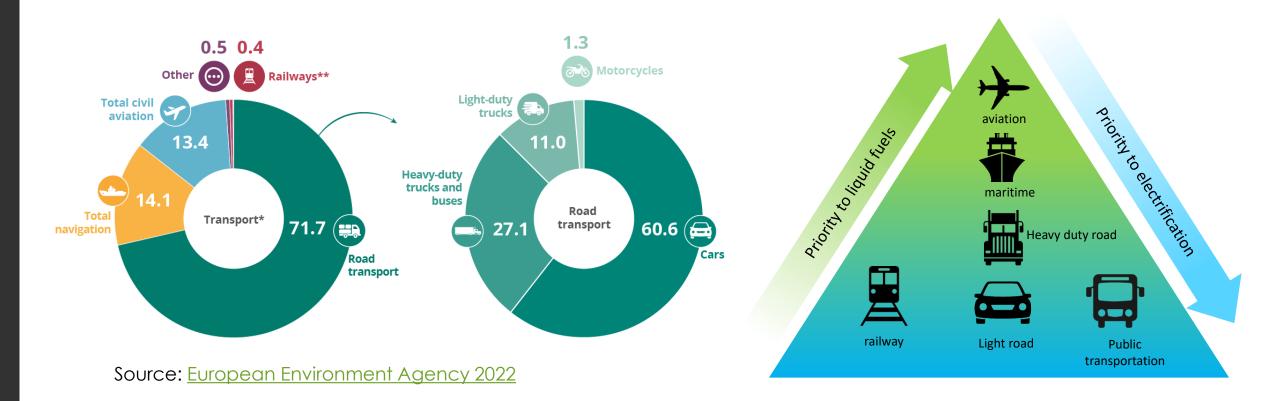


12th Stakeholder Plenary Meeting

12 March 2025, Brussels

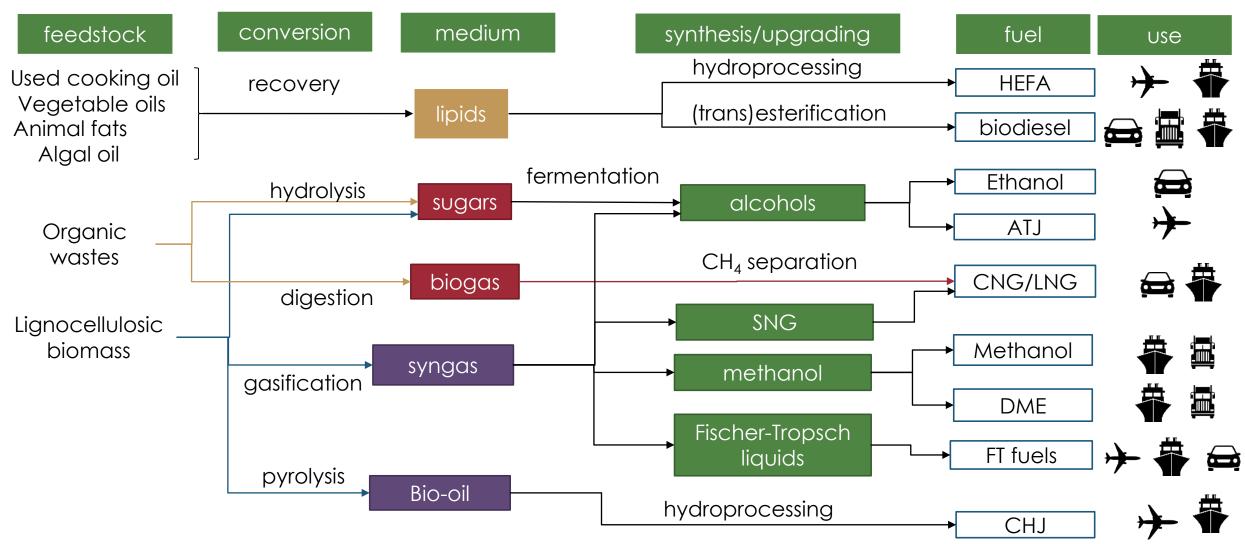
Biomass and sustainable transport

- Transport is responsible for about 25% of the EU's total CO₂ emissions
- The EU aims to reduce by 90% the greenhouse gas emissions from transport by 2050, compared with 1990
- Biofuels are crucial for reducing emissions in the transport sector
- Major role on the so-called "hard-to-abate sectors" aviation and maritime decarbonization



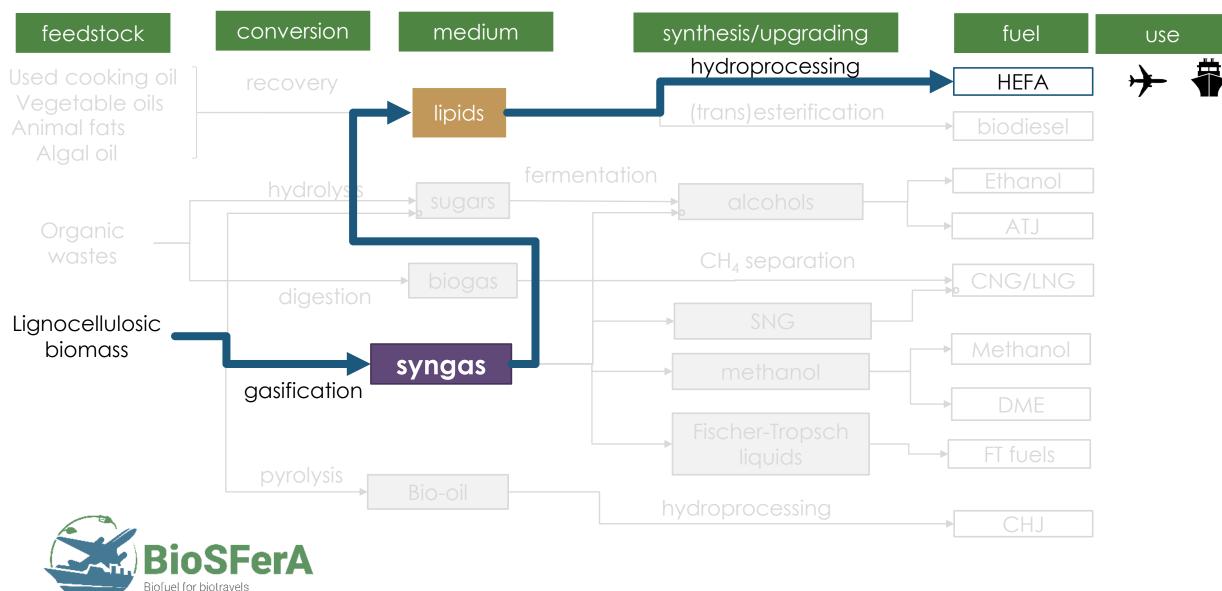
Advanced biofuels production pathways



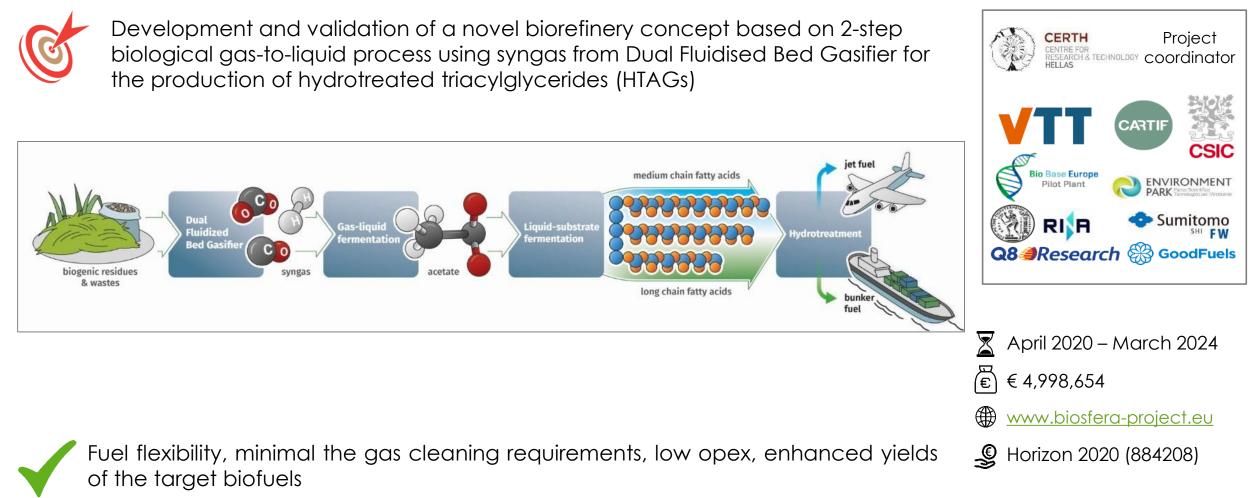


Advanced biofuels production pathways



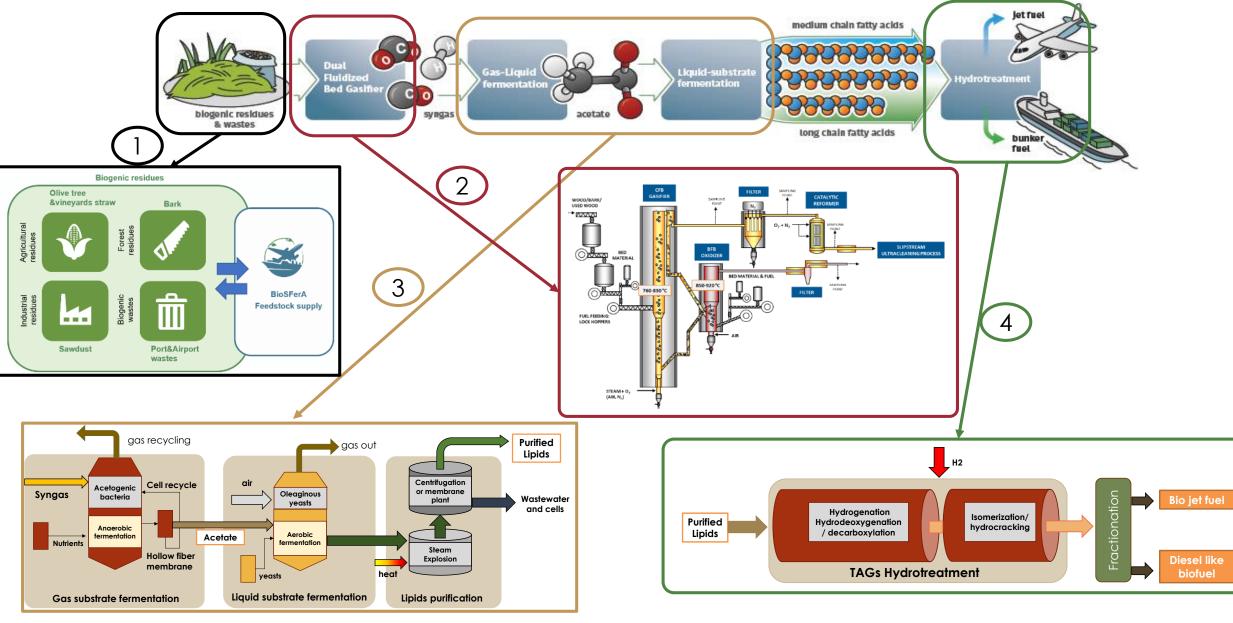




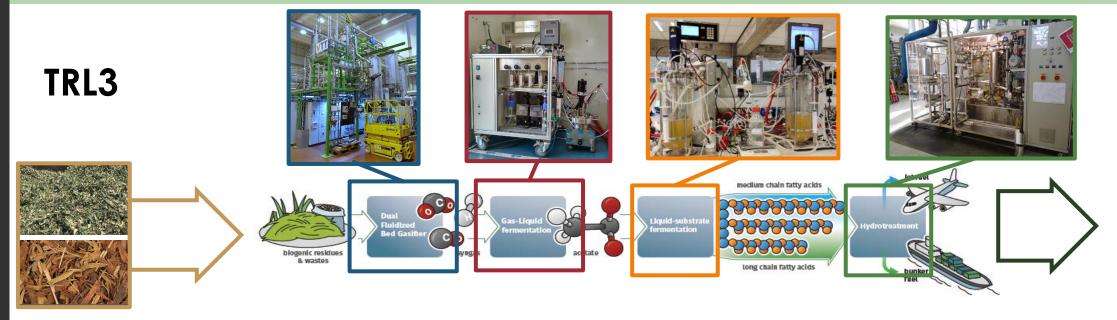




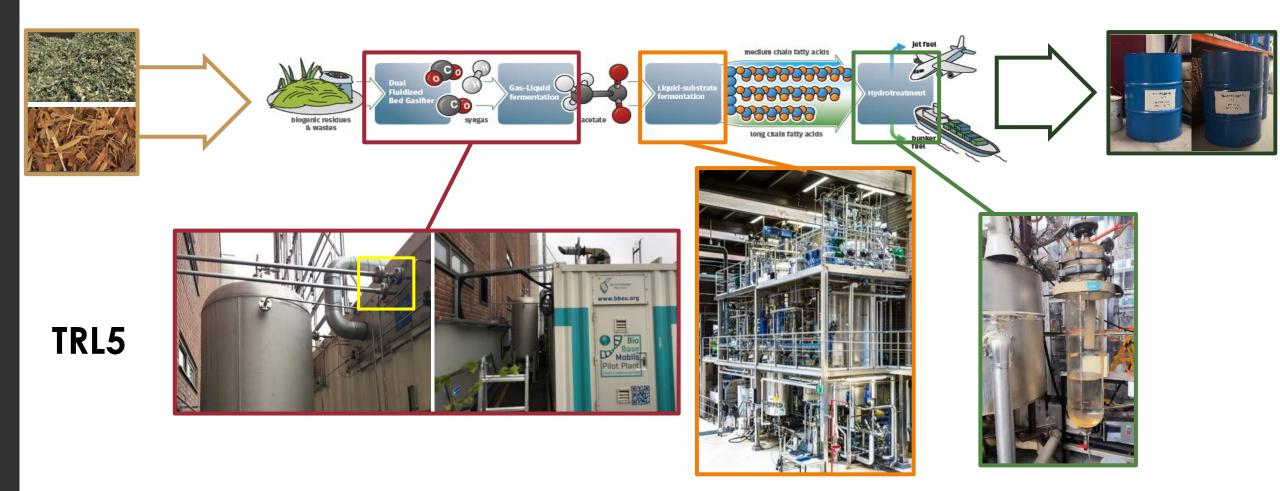








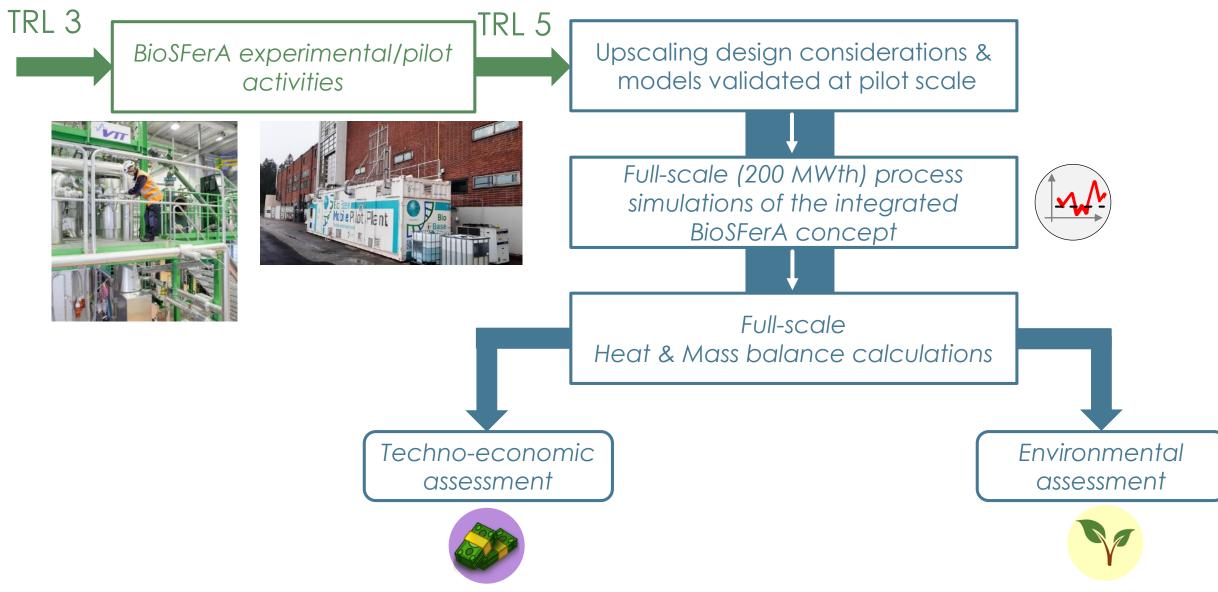




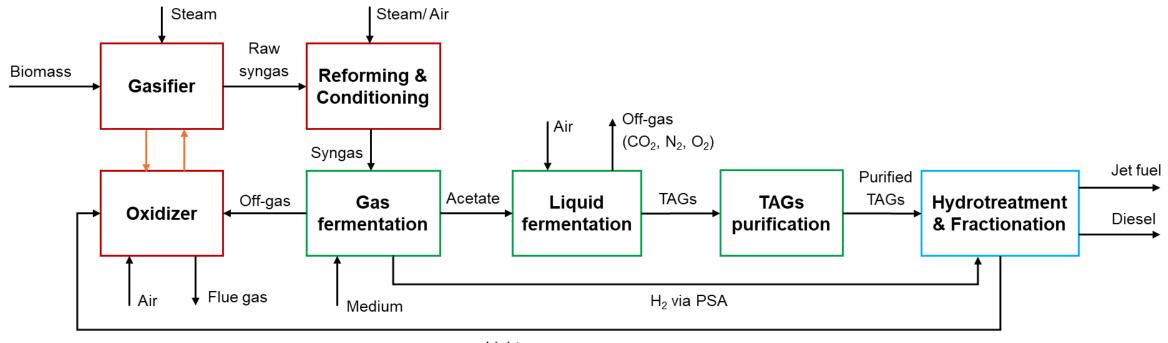
BioSFerA scale up and impact assessment



Methodology



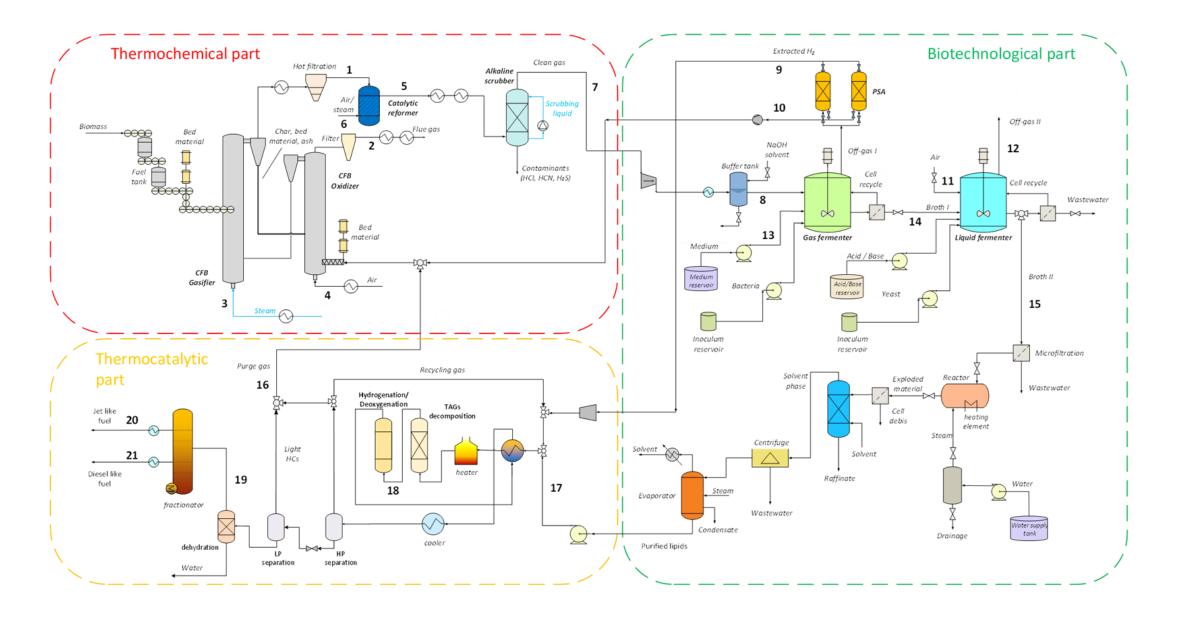
BioSFerA integrated concept



Light gases

- ➤ Utilization of the off-gas (unreacted gas) of the gas fermentation in the oxidizer of the DFBG unit → higher gasification efficiency, avoidance of technical barriers related to internal gas recycle in the bioreactor (i.e. inerts/contaminants accumulation)
- Internal hydrogen extraction (and supply to the hydrotreatment unit) from the off-gas of the anaerobic fermentation via PSA (Pressure Swing Adsorption) -> avoidance of such an energy/cost-consuming unit like an electrolyzer
- Air-driven autothermal reforming of syngas hydrocarbons instead of oxygen-driven, since in the absence of gas recycle in the bioreactor, some nitrogen content in the reformed gas would not be a critical problem -> avoidance of operational costs related to external purchase of industrial oxygen

BioSFerA process flow diagram at industrial scale

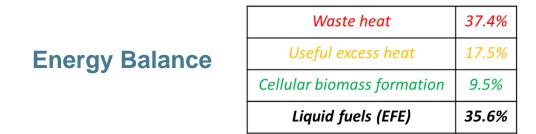


Full-scale (200 MW_{th}) process simulations



- Energetic Fuel Efficiency (EFE) is the fraction of the chemical energy in the initial feedstock that is transferred to the final fuels
- > Carbon Utilization (CU) is the fraction of carbon in initial feedstock that is converted to the final fuels
- > Liquid Fuel mass yield is the mass flow ratio of liquid fuels (products) to biomass feedstock (feed)

Parameter	Unit	Value (simulation output)
Feed (crushed bark)	t/h	40.46
Liquid product (jet fuel)	t/h	2.56
Liquid product (diesel)	t/h	2.88
Cellular biomass (by-product)	t/h	1.21
Electric power demand	MWel	8.20
Energetic Fuel Efficiency (EFE)	%	35.60
Carbon Utilization (CU)	%	25.40
Liquid Fuel mass yield (kg _{product} /kg _{feed})	%	13.44



Carbon Balance	Biogenic CO ₂	
	Wastewater	
	Cellular biomass for	

Liquid fuels (CU)	25.4%
Cellular biomass formation	5.6%
Wastewater	1.1%
Biogenic CO_2	67.9%

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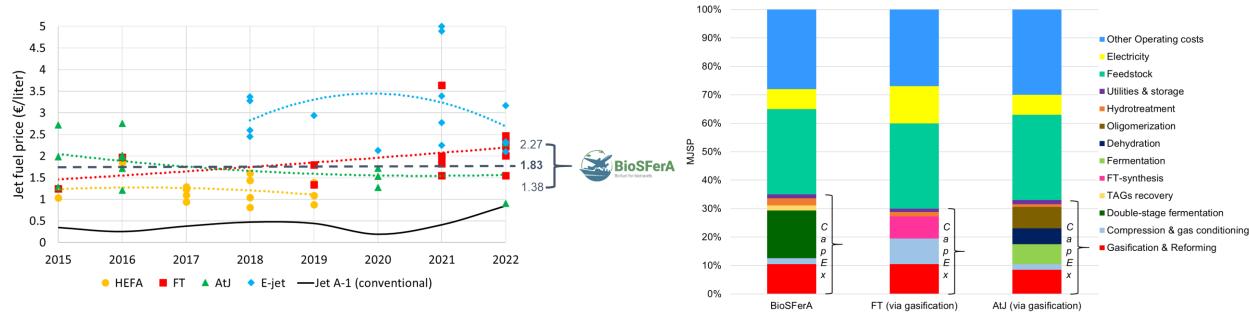
Business cases – Main results

Business case	Jet Fuel scenario	Marine fuel scenario	Microbial oil scenario
Total Capital Investment (€)	576,928,000	557,568,000	526,592,000
Annual operating costs (€/year)	49,984,760	49,509,560	48,749,240
Income from diesel (€/year)	14,475,024	-	-
Income from cellular biomass (€/year)	6,288,716	6,288,716	6,288,716
Biomass feed (t/year)	301,295	301,295	301,295
Produced jet fuel (t/year)	32,435	-	-
Produced diesel (t/year)	8,042	40,744	-
Produced microbial oil (†/year)	-	-	50,395
Minimum Jet Selling Price - MJSP (€/L)	1.83	-	-
Minimum Diesel Selling Price - MDSP (€/L)	-	1.71	-
Minimum Oil Selling Price - MOSP (€/L)	-	-	1.32

Techno-economic assessment



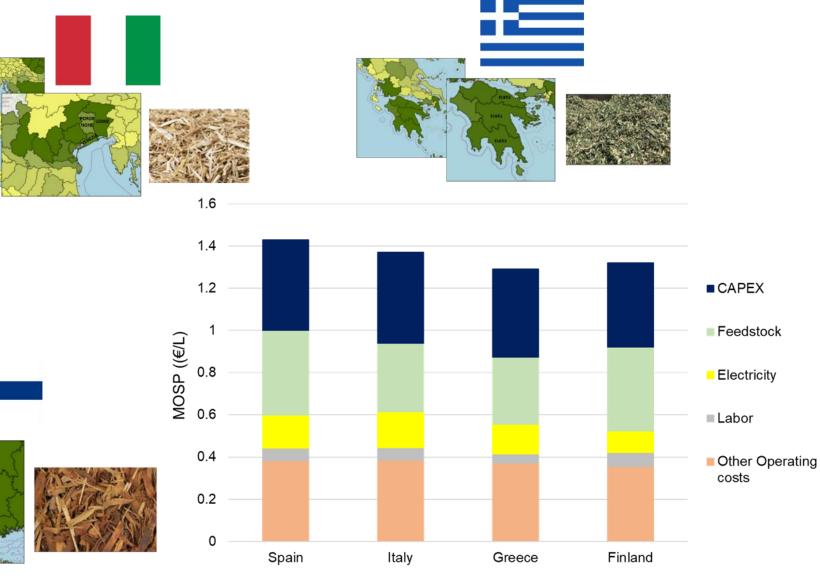
Benchmarking with the dominant biofuel (jet) technologies



- ► HEFA-produced SAF is the most cost-competitive option and the only route so far that can consistently compete with conventional jet fuel prices. The respective trend lines for the semi-commercialized Fischer-Tropsch (FT) and Alcohol-to-Jet (AtJ) routes lie well within the range of 1.50-2.00 €/L.
- ➤ The obtained baseline MJSP of 1.83 €/L reveals the preliminary ability of the BioSFerA concept to be financially competitive since it is within the range (1.50-2.00 €/L) of the dominant BtL technologies (FT & AtJ).
- The capital investment of the BioSFerA concept seems as demanding as for the other technologies, mainly due to the large required number of bioreactors. Higher obtained productivities and concentrations for acetic acid/TAGs production can drastically reduce the capital costs of the double-stage fermentation and upgrade the financial competitiveness of the concept.

Techno-economic assessment

Replication pre-feasibility studies in 4 EU countries



Environmental assessment

Life Cycle Assessment (LCA) framework

Scope

Evaluation of the environmental impact of 5 different scenarios throughout their entire life cycle - different types of biomass feedstock and biorefinery locations are considered.

Methodology

Guidelines & modelling framework in accordance with the European Renewable Energy Directive 2018/2001/EU (RED II) & the ISO 14040/44 Standards.

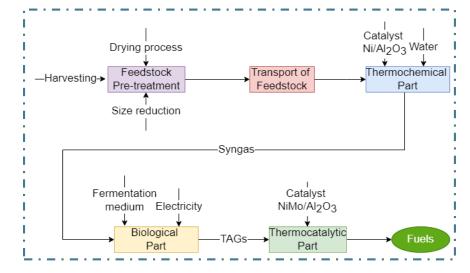
System boundaries

All stages of BioSFerA project are considered in the analysis;

- Feedstock pre-treatment stage (harvesting, drying, chopping)
- Thermochemical part / biomass-to-syngas
- Compression stage / prior to fermentation process
- Biological part / syngas-into-TAGs
- Purification of TAGs & Thermocatalytic part / TAGs-into-liquid fuels



Simplified definition of system boundaries



Investigated Scenarios

Country	Feedstock
Finland	Crushed bark
Greece – Case 1*	Olive tree pruning & organic waste (80/20 w/w DM)
Greece – Case 2	Olive tree pruning
Italy	Cereal straw
Spain	Vineyard pruning

*Drying process is only included in Case 1 of Greek scenario (high moisture content of organic waste 70-75%)



Environmental assessment

LCA Results

Achievement

50-86 % GHG emission savings are achieved compared to the fossil fuel comparator (as defined in RED II Directive).

Major findings

Results are strongly affected by the (a) electricity consumption for the compression stage, (b) natural gas for the drying process (organic waste scenario) & (c) nutrients utilization for the fermentation.

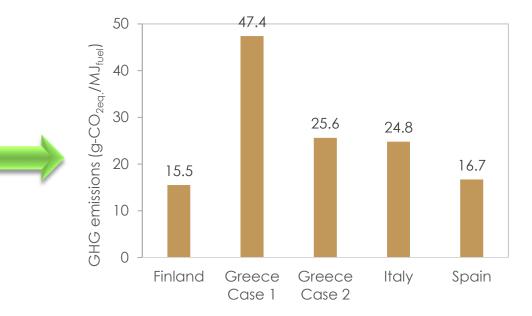
BioSFerA LCA results are <u>consistent</u> & <u>competitive</u> with the ones reported in similar cases in the relevant literature.

Future perspective

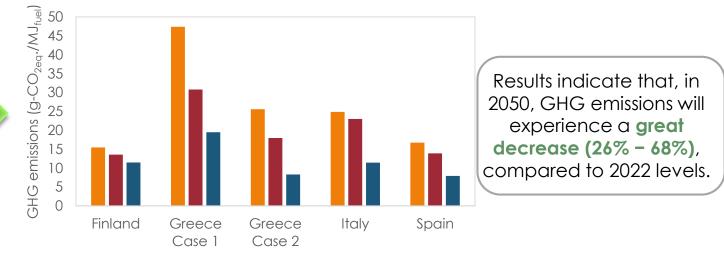
Effect of potential increase of RES share on GHG emissions;

- By 2030, around 70% of RES in each country's electricity generation mix is expected and
- ✓ by 2050, around 100% of RES is expected.

Results are calculated considering each country's National Energy And Climate Plan.



■2022 ■2030 ■2050

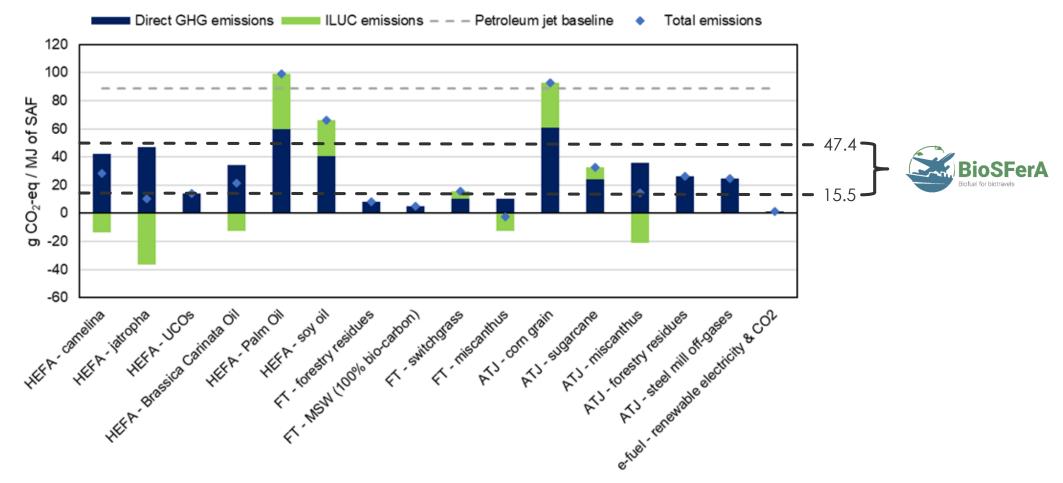




Environmental assessment



Benchmarking with the dominant biofuel (jet) technologies



Conventional jet fuel produced from petroleum resources, has a carbon intensity within the range of 85-95 g CO2eq/MJ. BioSFerA's measured carbon footprint lies in the range of 15.5 – 47.4 g CO2eq/MJ, achieving 50-86% GHG emission savings compared to conventional jet fuel.

What is next?



Accelerating the sustainable production of advanced biofuels and RFNBOs - from feedstock to end-use: the **FUELPHORIA** project



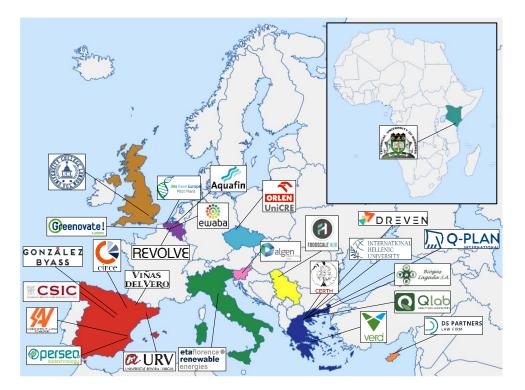
- Duration: 1/10/2023 30/09/2027 (48 Months)
- ě
- Coordinator:



• Beneficiaries: 22, Affiliated Entities: 3, Associated Partners: 1

Budget/ EU contribution: €11,144,321.30/ €9,678,598.55

• <u>https://fuelphoria.eu/</u>



OBJECTIVES

- Demonstrate robust and cost-effective technological solutions for the production of advanced biofuels & RFNBOs
- Build a portfolio of sustainable, secure & complete Value Chains for advanced biofuels and RFNBOs from feedstock to end use
- Promote the exploitation of advanced biofuels and RFNBOs
 - by identifying barriers in value chains at EU level and in Africa
 - through policy recommendations at EU level
 - through new business and marketing concepts in Europe and Africa

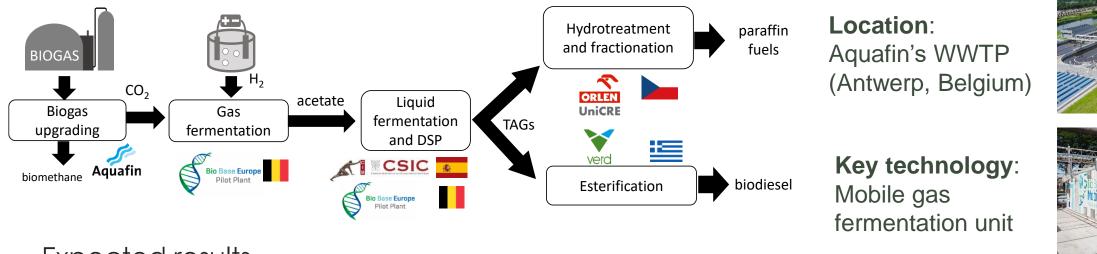
Accelerating the sustainable production of advanced biofuels and RFNBOs - from feedstock to end-use: the **FUELPHORIA** project



Demos overview BIOOS BIOGS FEEDSTOCK **BIOGAS PLANT** WINERY PLANT **BIOGAS PLANT** WASTE TREATMENT PLANT SUPPLIER FEEDSTOCK DIGESTATE / CO. **ORGANIC URBAN WASTE** i -Lipids Fermentation Hydrogenation 2-step extraction 🖌 and catalytic fermentation with green H, from algae process PARAFFIN н **FINAL PRODUCT** BIODIESEL BIODIESEL ETHANOL METHANOI r. τ. 1 POWER AT ι. **AVIATION /** ROAD ROAD GAS FIRED ROAD **END USER** ISLAND ENERGY **ROAD TRANSPORT** 1.1 MARITIME TRANSPORT TRANSPORT POWER PLANT TRANSPORT SYSTEMS 00 0 00 0 00 0

DEMO 1 description





Expected results

- 75 kg biogenic CO2 will be converted into advanced liquid renewable fuel
- 30-day gas fermentation run with the mobile unit: 75 kg CO₂ in total
- Up to 90% of CO_2 conversion at the fermenter
- Hundreds of kilos of TAGs produced at the second fermenter
- Acetate concentration 25-30 g/L after the first fermentation step
- Lipids concentration 50-100 g/L after the second fermentation step
- 150L of liquid paraffinic fuel from microbial oil hydroprocessing
- 100L of biodiesel produced from microbial oil esterification

- Introduction of a new sustainable feedstock for HEFA plants, expanding the portfolio of advanced feedstocks for marine and SAF
- 35.6% energy efficiency, 25.4% total C utilization
- Baseline MJSP: 1.83 €/L
- GHG emission savings: 48% to 86% compared to conventional fossil fuels
- Most environmental case: GHG emissions at 15.5 g CO2_{eq}/MJ_{fuel}
- New endeavor at demo scale for turning biogenic CO₂ into microbial oil for marine fuels and SAF

Thank you!







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